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IN THE CLAIMS

1. (Cancelled)
2. (Currently Amended) The catalyzed adsorber of Claim 484, wherein the substrate is a cordierite monolith material.
3. (Currently Amended) The catalyzed adsorber of Claim 484 wherein the overlayer has a thickness less than about 30 microns.
4. (Currently Amended) The catalyzed adsorber of Claim 484, wherein the underlayer further comprises an inorganic oxide.
5. (Original) The catalyzed adsorber of Claim 4, wherein the inorganic oxide is alumina.
6. (Currently Amended) The catalyzed adsorber of Claim 484, wherein the overlayer non-catalyst loading is about 0.8 to about 1.0 g/in³.
7. (Original) The catalyzed adsorber of Claim 6, wherein the overlayer non-catalyst loading is about 0.9 to about 1.0 g/in³.
8. (Cancelled)
9. (Currently Amended) The catalyzed adsorber of Claim 488, wherein the overlayer has a catalyst loading of about 0.1 to about 0.25 g/in³.
10. (Currently Amended) The catalyzed adsorber of Claim 484, wherein the overlayer has a catalyst loading of about 0.1 to about 0.2 g/in³.

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11. (Currently Amended) The catalyzed adsorber of Claim 48+, wherein the catalyst is selected from the group consisting of palladium, platinum, rhodium, and mixtures and alloys comprising at least one of the foregoing catalysts.

12-14. (Cancelled)

15. (Currently Amended) The catalyzed adsorber of Claim 48+, wherein the overlayer further comprises an inorganic oxide.

16. (Original) The catalyzed adsorber of Claim 15, wherein the inorganic oxide is selected from the group consisting of alumina, silica, titania, magnesia, zirconia, beryllia, ceria, lanthana, zirconia, and compounds and mixtures comprising at least one of the foregoing inorganic oxides.

17. (Original) The catalyzed adsorber of Claim 16, wherein the inorganic oxide is selected from the group consisting of delta phase alumina, gamma phase alumina, and combinations comprising at least one of the foregoing inorganic oxides.

18. (Original) The catalyzed adsorber of Claim 17, wherein the inorganic oxide is lanthanum stabilized gamma phase alumina.

19. (Currently Amended) A method for making a catalyzed adsorber system for treating exhaust gas, comprising:

providing a substrate;

disposing a zeolite underlayer over the substrate, the zeolite is a faujasite having a Si/Al ratio of about 3.0 to about 10; and

disposing a catalyst overlayer over the underlayer, wherein the overlayer is zeolite free, wherein an overlayer non-catalyst loading is less than about 1.0 g/in³, and wherein an overlayer catalyst loading is about 0.1 to about 0.5 g/in³.

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20. (Previously Presented) The method for making the catalyzed adsorber as in Claim 19, wherein the overlayer non-catalyst loading is about 0.8 to about 1.0 g/in³.

21. (Original) The method for making the catalyzed adsorber as in Claim 20, wherein the overlayer non-catalyst loading is about 0.9 to about 1.0 g/in³.

22. (Cancelled)

23. (Previously Presented) The method for making the catalyzed adsorber as in Claim 22, wherein the overlayer has a catalyst loading of about 0.1 to about 0.25 g/in³.

24. (Previously Presented) The method for making the catalyzed adsorber as in Claim 19, wherein the overlayer has a catalyst loading of about 0.1 to about 0.2 g/in³.

25. (Previously Presented) The method for making the catalyzed adsorber as in Claim 19, wherein the catalyst is selected from the group consisting of palladium, platinum, rhodium, and mixtures and alloys comprising at least one of the foregoing catalysts.

26. (Original) The method for making the catalyzed adsorber as in Claim 19, wherein the overlayer comprises less than about 3% zeolite.

27. (Cancelled)

28. (Original) The method for making the catalyzed adsorber as in Claim 19, wherein the overlayer further comprises an inorganic oxide.

29. (Original) The method for making the catalyzed adsorber as in Claim 28, wherein the inorganic oxide is selected from the group consisting of alumina, silica, titania, magnesia, zirconia, beryllia, ceria, lanthana, zirconia, and compounds and mixtures comprising at least one of the foregoing inorganic oxides.

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30. (Original) The method for making the catalyzed adsorber as in Claim 29, wherein the inorganic oxide is selected from the group consisting of delta phase alumina, gamma phase alumina, and combinations comprising at least one of the foregoing inorganic oxides.

31. (Original) The method for making the catalyzed adsorber as in Claim 30, wherein the inorganic oxide is lanthanum stabilized gamma phase alumina.

32-33. (Cancelled)

34. (Currently Amended) The catalyzed adsorber of Claim ~~48~~⁴, wherein the zeolite has a sodium content of less than 0.1 wt.% of the total weight of the zeolite.

35. (Previously Presented) The method of Claim 19, wherein the zeolite has a sodium content of less than 0.1 wt.% of the total weight of the zeolite.

36. (Cancelled)

37. (Currently Amended) The catalyzed adsorber of Claim ~~49~~³⁶, wherein the overlayer non-catalyst loading is about 0.8 to about 1.0 g/in³.

38. (Currently Amended) The catalyzed adsorber of Claim ~~49~~³⁶, wherein the overlayer non-catalyst loading is about 0.9 to about 1.0 g/in³.

39. (Currently Amended) The catalyzed adsorber of Claim ~~49~~³⁶, wherein the catalyst is selected from the group consisting of palladium, platinum, rhodium, and mixtures and alloys comprising at least one of the foregoing catalysts.

40-41. (Cancelled)

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42. (Currently Amended) The catalyzed adsorber of Claim 4936, wherein the overlayer further comprises an inorganic oxide.

43. (Currently Amended) The catalyzed adsorber of Claim 4936, wherein the underlayer is noble metal free.

44. (Currently Amended) The catalyzed adsorber of Claim 484, wherein the underlayer is noble metal free.

45. (Previously Presented) The method of Claim 19, wherein the underlayer is noble metal free.

46-47. (Cancelled)

48. (New) A catalyzed adsorber for treating exhaust gas, comprising:
a substrate;
a zeolite underlayer disposed over the substrate, wherein the zeolite is a faujasite having a Si/Al ratio of about 3.0 to about 10; and
a catalyst overlayer disposed over the underlayer, wherein the overlayer is zeolite free comprising less than about 3% zeolite, wherein an overlayer non-catalyst loading is less than about 1.0 g/in³, and wherein an overlayer catalyst loading is about 0.1 to about 0.5 g/in³.

49. (New) A catalyzed adsorber for treating exhaust gas, comprising:
a substrate;
a zeolite underlayer disposed over the substrate, wherein the zeolite is a faujasite having a Si/Al ratio of about 3.0 to about 10, and wherein the zeolite has a sodium content of less than 0.1 wt.% of the total weight of the zeolite; and
a catalyst overlayer disposed over the underlayer, wherein the overlayer is zeolite free, wherein an overlayer non-catalyst loading is less than about 1.0 g/in³, and wherein an overlayer catalyst loading is about 0.1 to about 0.5 g/in³.

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50. (New) A method for making a catalyzed adsorber system for treating exhaust gas, comprising:

providing a substrate;

disposing a zeolite underlayer over the substrate, wherein the zeolite is a faujasite having a Si/Al ratio of about 3.0 to about 10, wherein the zeolite has a sodium content of less than 0.1 wt.% of the total weight of the zeolite; and

disposing a catalyst overlayer over the underlayer, wherein the overlayer is zeolite free, wherein an overlayer non-catalyst loading is less than about 1.0 g/in^3 , and wherein an overlayer catalyst loading is about 0.1 to about 0.5 g/in^3 .